

Failure Prediction of Spool Control Valve using CFD Simulation

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Keywords: Failure Prediction, Spool Control Valve, CFD Simulation

Abstract. Spool control valves play an important role in fluid power systems and required high reliability. Prediction of possible failures for such valves is a key issue. According to research most of failures which may appear are caused by contaminated fluid. Contaminants of fluid may cause erosion of metallic surfaces or cavitation wear. Both types of wear may be predicted by using CFD simulation tools and multiphase flow which includes phase changes and possibility of simulation of flow with solid particles.

Introduction

Failures prediction for hydraulic valve is very important issue due to the fact that its malfunction may cause human injuries or environmental pollution. Among all causes of hydraulic systems failures, contamination of hydraulic fluid is one of the most common. It is estimated that majority (up to 90%) of failures is caused by contamination of hydraulic fluid which might be solid particles (remaining of wear or dust) or chemical agents (liquids or gases). It is not possible to prevent hydraulic fluid against contamination even using sophisticated filtration systems. Contamination may appear in the hydraulic systems internally as a normal process of operation, as a result of wear of hydraulic components. Solid particles in very specific flow conditions, very often with high flow velocity, gain momentum from fluid and may cause erosive wear inside components. Additionally, fluid flowing inside hydraulic components, particularly inside valves, rapidly changing direction and velocity what may lead to sudden pressure drop, below saturation pressure and cavitation and wear of surface of valve components. Both type of wears: erosive and cavitation has been investigated from decades on experimental way. Recent development of simulation methods (in particular computational fluid dynamics: CFD) allows to predict wear before their occurrence [1-4]. This paper presents research on flow inside spool control valve for two cases. First one is multiphase flow with contaminants (metallic particles) while the second deals with phase change flow (cavitation). Both simulations might be used for predicting spool valve wear.

The failure prediction presented here can be used in analogous issues, both related to fluid flows (e.g. biotechnology [5, 6], heat flows [7]) and in the field of solid materials engineering (e.g. materials science [8, 9] and design of medical implants [10]) as well as enhancement of surface layers [11], where the aim is to improve tribological properties [12] and fatigue resistance [13]. It is certain that this will have an impact on related methods of management

optimization [14, 15] and data analysis [16, 17] as well as CFD numerical methods [18-20] aimed at erosion modeling [21, 22] and associated failure analysis methods [23, 24].

Modelling of erosion and cavitation

The wear caused by impact of solid particles on walls for metals is a function of impact angle and particle velocity [25]:

$$E = kV_p^n f(\gamma) \tag{1}$$

where:

- E – dimensionless mass (mass of eroded wall material divided by the mass of particle),
- V_p – particle velocity,
- n – exponent value which for metals is between 2.3 and 2.5,
- $f(\gamma)$ – function of impact angle.

One of the models that describes rate of wear is Finnie model [26] :

$$E = kV_p^2 f(\gamma) \tag{2}$$

where:

$$f(\gamma) = \frac{1}{3} \cos^2(\gamma) \text{ if } \tan(\gamma) > \frac{1}{3} \tag{3}$$

$$f(\gamma) = \sin(2\gamma) - 3\sin^2(\gamma) \text{ if } \tan(\gamma) > \frac{1}{3} \tag{4}$$

Other model which describes erosion rate is Tabakoff and Grant [27]:

$$E = k_1 f(\gamma) V_p^2 \cos^2(\gamma) [1 - R_T^2] + f(V_{PN}) \tag{5}$$

where:

$$f(\gamma) = \left[1 + k_2 k_{12} \sin \left(\gamma \frac{\pi}{\gamma_0} \right) \right]^2 \tag{6}$$

$$R_T = 1 - k_4 V_p \sin(\gamma) \tag{7}$$

$$f(V_{PN}) = k_3 \left(V_p \sin(\gamma) \right)^4 \tag{8}$$

$$k_2 = \begin{cases} 1.0 & \text{if } \gamma \leq 2\gamma_0 \\ 0 & \text{if } \gamma > 2\gamma_0 \end{cases} \tag{9}$$

k_1, k_{12} – constants.

Simulation of particles in continuous fluid in CFD is treated as two phases flow: discrete one (particles) and continuous one (fluid). Discrete particles are tracked into fluid domain during fluid flow. Equation of motion for a single particle according to Basset, Boussinesq and Oseen may be presented in the following way:

$$m_p \frac{dU_p}{dt} = F_D + F_B + F_R + F_{VM} + F_P + F_{BA} \tag{10}$$

where: F_D – drag force, F_B – buoyancy force, F_R – Coriolis force, F_{VM} – is inertia force of fluid occupied by particle (Virtual Mass), F_P – pressure force, F_{BA} – Basset force

The inertia force of fluid occupied by particle (Virtual Mass) is expressed by the following equation:

$$F_{VM} = \frac{c_{VM}}{2} m_F \left(\frac{dU_F}{dt} - \frac{dU_P}{dt} \right) \quad (11)$$

Transforming Eq. 10 we obtain:

$$\frac{dU_P}{dt} = \left(\frac{1}{m_P + \frac{c_{VM}}{2} m_F} \right) (F_D + F_B + F_R + F'_{VM} + F_P + F_{BA}) \quad (12)$$

where

$$F'_{VM} = \frac{c_{VM}}{2} m_F (U_F \nabla U_F) \quad (13)$$

$$m_P = \frac{\pi}{6} d_p^3 \rho_P \quad - \text{particle mass,}$$

$$m_F = \frac{\pi}{6} d_p^3 \rho_F \quad - \text{fluid mass,}$$

$$d_p \quad - \text{the particle diameter,}$$

$$\rho_P, \rho_F \quad - \text{density of particle and fluid respectively.}$$

Assuming that:

$$R_{VM} = \frac{m_P}{m_P + \frac{c_{VM}}{2} m_F} = \frac{\rho_P}{\rho_P + \frac{c_{VM}}{2} \rho_F} \quad (14)$$

Finally Eq. 10 has the following form:

$$\frac{dU_P}{dt} = \left(\frac{R_{VM}}{m_P} \right) (F_D + F_B + F_R + F'_{VM} + F_P + F_{BA}) \quad (15)$$

In generally, tendency of fluid flow to cavitation may be expressed as:

$$c_a = \frac{p - p_v}{0.5 \rho U^2} \quad (16)$$

One of the approaches which describes bubble dynamics is The Rayleigh-Plesset formula:

$$R_b \frac{d^2 R_b}{dt^2} + \frac{3}{2} \left(\frac{dR_b}{dt} \right)^2 + \frac{2\sigma}{\rho R_b} = \frac{p_v - p}{\rho} \quad (17)$$

After neglecting surface tension and term of second order the above eq. have the following form:

$$\frac{dR_b}{dt} = \sqrt{\frac{2}{3} \left(\frac{p_v - p}{\rho} \right)} \quad (18)$$

The rate of changes of bubble volume is:

$$\frac{dV_b}{dt} = 4\pi R_b^2 \sqrt{\frac{2}{3} \left(\frac{p_v - p}{\rho} \right)} \quad (19)$$

The rate of changes of bubble mass is:

$$\frac{dm_g}{dt} = 4\pi R_b^2 \rho_g \sqrt{\frac{2}{3} \left(\frac{p_v - p}{\rho} \right)} \quad (20)$$

The number of bubbles Nb per unit volume rg is expressed by:

$$r_g = \frac{4}{3} \pi R_b^2 N_b \quad (21)$$

The total interphase mass transfer per unit volume is:

$$\dot{m}_{fg} = 3 \frac{r_g \rho_g}{R_b} \sqrt{\frac{2}{3} \frac{p_v - p}{\rho_f}} \quad (22)$$

After including condensation to above expression have the following form:

$$\dot{m}_{fg} = 3F \frac{r_g \rho_g}{R_b} \sqrt{\frac{2}{3} \frac{p_v - p}{\rho_f}} \operatorname{sgn}(p_v - p) \quad (23)$$

And finally the vapor transport equation have form:

$$\frac{\partial}{\partial t} (\alpha \rho_v) + \nabla \cdot (\alpha \rho_v \mathbf{U}_v) = R_e - R_c \quad (24)$$

where:

R_b – bubble radius, p_v – vapor pressure, p – pressure of liquid surrounding the bubble, ρ – liquid density, ρ_g – vapor density, σ – surface tension, U_v – vapour phase velocity, α – vapor volume fraction, n – bubble number, R – phase change rate, f_v – vapor mass fraction, f_g – noncondesable gases, R_e, R_c – mass transfer source terms connected to the growth and collapse of the vapor bubbles, respectively.

Spool control valve

The spool control valve presented in Fig. 1. is used to control the direction of flow and movements speed of actuators. Position of spool is determined by proportional solenoids which allows to control both direction of flow and receivers movement speed. Return to neutral position (any receiver is supplied) is provided by two springs. The shape of the spool determines flow configuration (connections between ports: P, T, A, B).

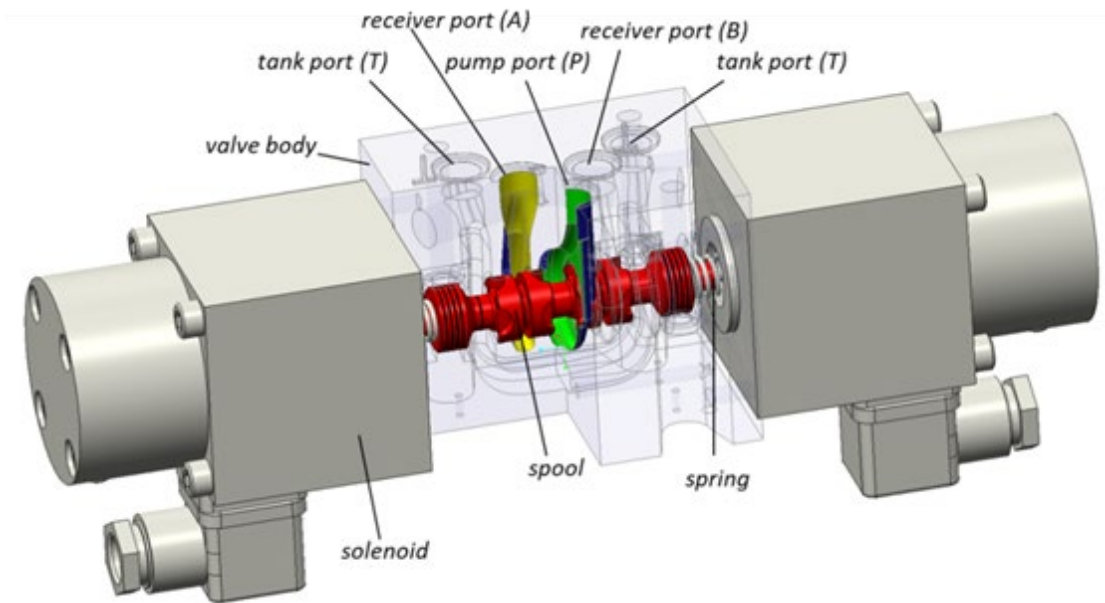


Fig. 1. Spool control valve.

CFD analysis of flow control valve

CFD simulations were conducted in Ansys CFX a general purpose CFD code, which use Finite Volume Method (FVM) for solving flow governing equations and applies multiphase flow model with phase change and Lagrangian particle tracking modelling technique. For numerical simulation path P-A was used with initial opening of 0.3 mm. Boundary conditions and grid is presented in Fig. 3. CFD simulations were performed for cavitation and flow with solid particles independently.

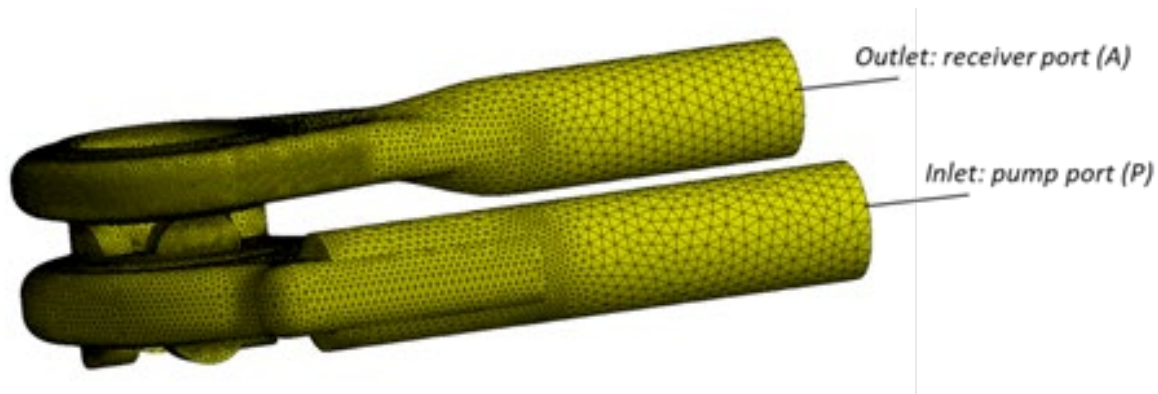


Fig. 2. CFD model: grid and boundary conditions.

CFD simulation was performed for fixed spool position for steady state conditions and for the following assumptions:

- Fluid (hydraulic oil) has a constant properties: density 880 [kg/m³], viscosity $\nu=40$ [mm²/s];
- Flow is turbulent: k- ω turbulence model was used;
- Model is in thermodynamics equilibrium, heat transfer is not included;

Cavitation simulation included below assumptions:

- Saturation pressure is set to 0.2 [bar];
- Fluid is homogeneous without any dissolved gases;

Whereas particle flow simulation included following assumptions:

- Particles have uniform shape (spheres with diameter 20 [μ m]) and constant properties, 20 particles in 1 [cm³];
- Erosion model: Finnie;
- Interaction of particles and fluid is fully coupled;
- Simulations were performed for metallic particles (steel);
- Particles are uniformly injected at inlet to the valve.

Exemplary CFD simulations for solid particle flow are presented in Fig. 3 and Fig. 4. There are presented pathlines of hydraulic oil colored by velocity values and trajectory of solid particles (grey lines).

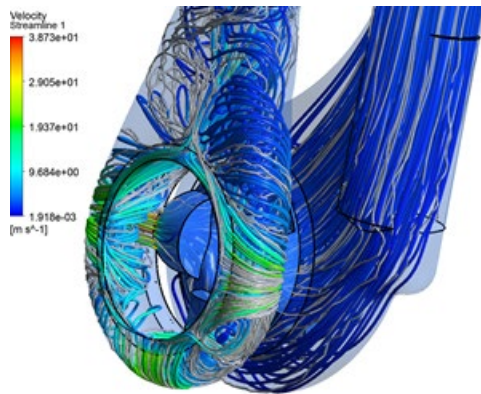


Fig. 3. Fluid path lines (color) and particles trajectory (grey).

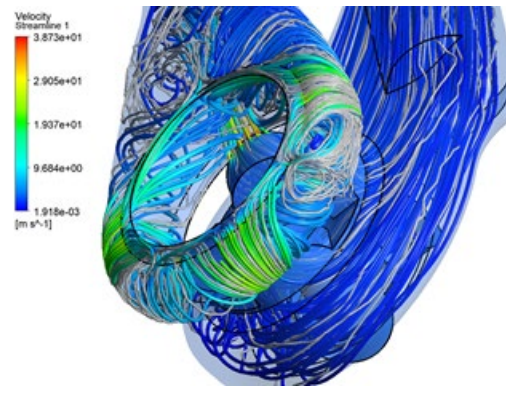


Fig. 4. Fluid path lines (color) and particles trajectory (grey).

Erosion rate density is presented in Fig. 5, which allows to identify areas which are exposed to erosion wear. Figure 6 presents distribution of gas fraction during fluid flow for given conditions.

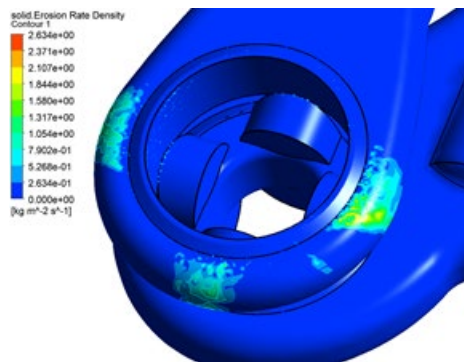


Fig. 5. Erosion rate density.

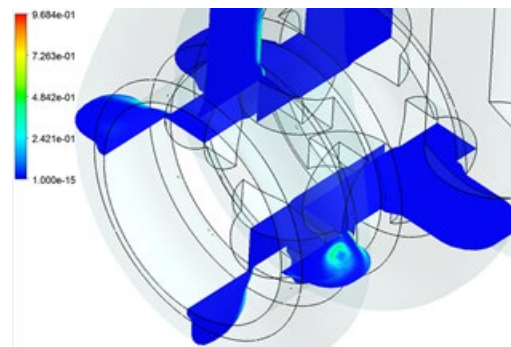


Fig. 6. Oil vapor fraction.

Conclusions

This paper presents attempt of failure prediction of spool control valve caused by contaminated fluid which may cause erosive or cavitation wear. Both are complex phenomena, however, available numerical simulation methods (CFD) allows conducting multiphase flows which includes phase changes (cavitation) and particle tracking. This paper presents simulation of flow inside spool valve for two cases, the first includes hydraulic fluids with metallic contaminants while the second flow with phase changes (cavitation). Obtained results allows to indicate areas which are mostly exposed on wear or to define flow conditions for which wear may occur. CFD simulation tools seem to be an effective tool for perdition of failures in fluid power components.

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